

Optimization and control of hyperbolic balance laws on networks for industrial applications

Günter Leugering

Benasque VII

Session:

Modeling, simulation and control for PDEs on graphs



FRIEDRICH-ALEXANDER
UNIVERSITÄT
ERLANGEN-NÜRNBERG

Department

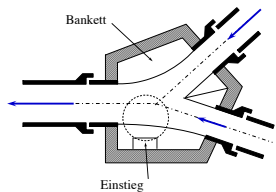
MATHEMATIK



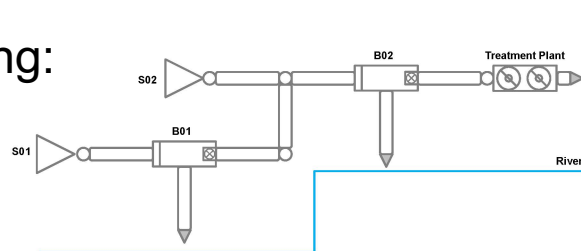
CONTINUOUS
OPTIMIZATION

Multiscale nature of the problem: waste water

PDE-modeling:
St. Venant's
system

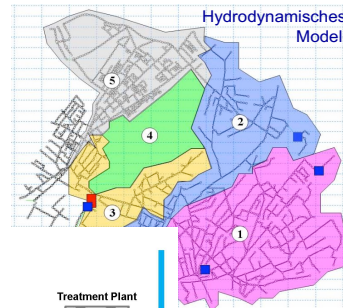


Homogenization
Effective models

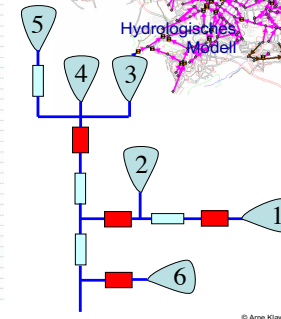


Subnet involving
Pumpes and valves

Realtime control
Discrete models



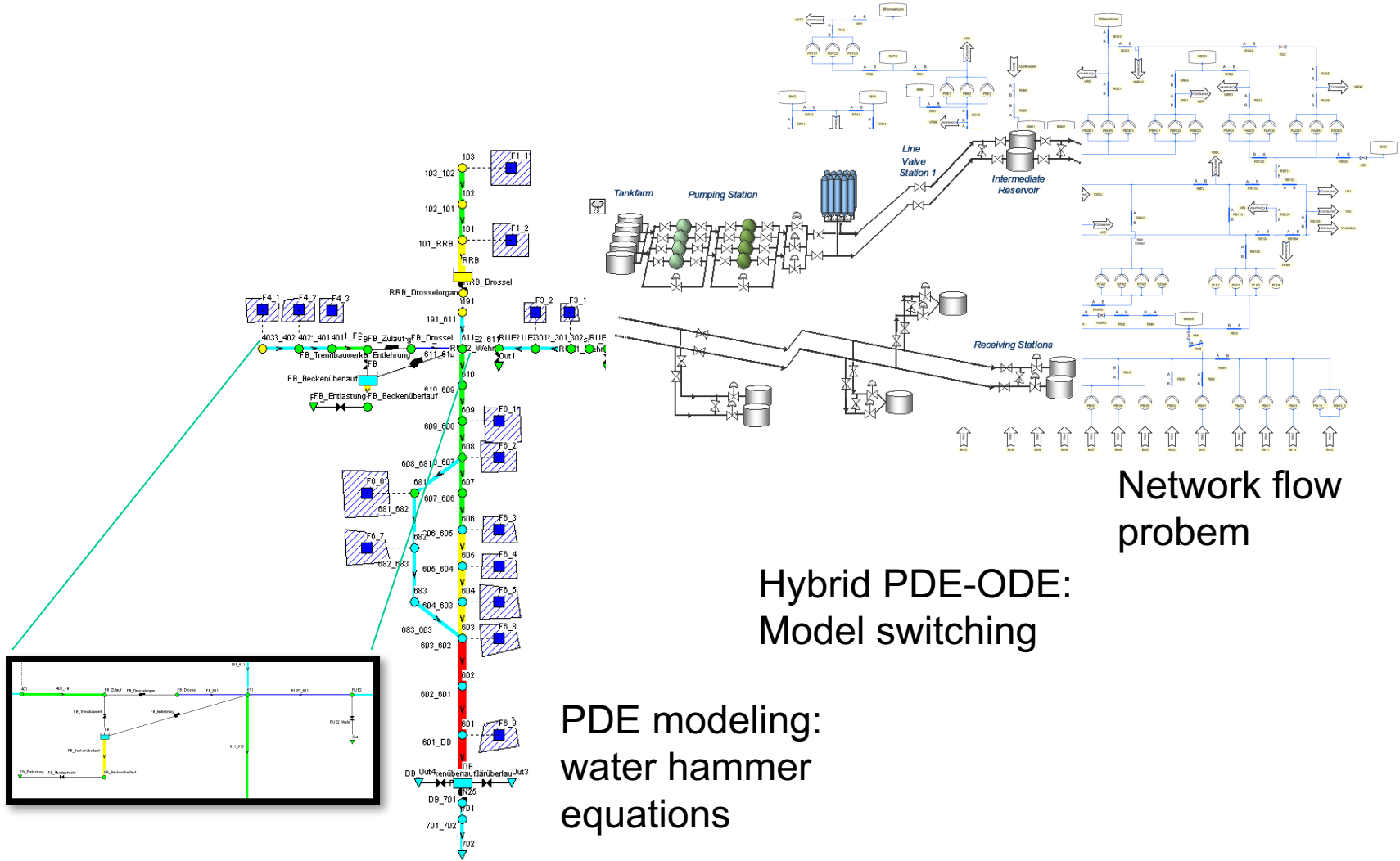
Coarse graining
Graph contraction



Finest level

Single pipes
and junctions

Multiscale modeling: fresh water systems

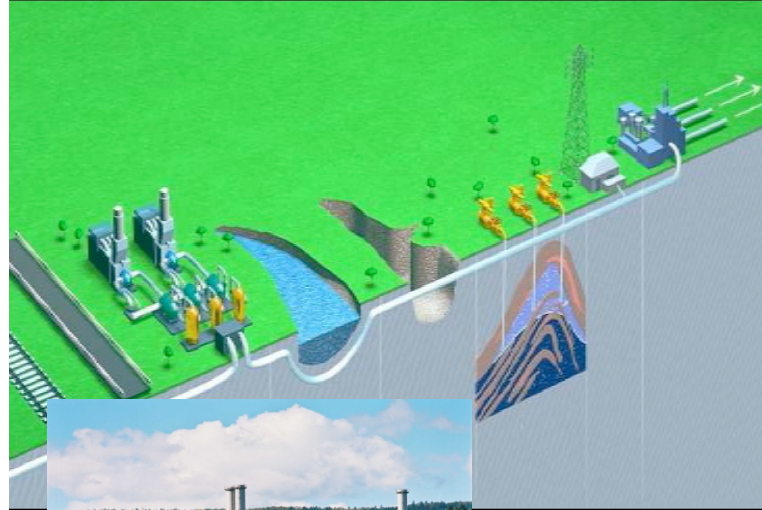


Gas-networks: Control of gas flow!

Gas-network in Germany:
DFG-research cluster
TRR154 since 2014

Industry: OGE

Individual pipe:
Parameters
(roughness, thickness,
bends, etc.)



,Global' network:
Effective model,
planning aspects

Subnetwork:
environment



Junctions:
Different pipes,
multijunctions

Compressors,
Valves, releases,
heaters

Control the gas flow from
suppliers to customers
by operating valves,
compressors, etc.
and thereby keep quality
and minimize cost!

General picture

$$\min_{(y,u,s) \in \Xi} I(y,u) := \sum_{i \in \mathcal{I}} \int_0^T \int_0^{\ell_i} l_i(y_i) dx dt + \frac{\nu}{2} \sum_{j \in \mathcal{J}^s \cup \mathcal{J}^c} \int_0^T |u_j(t)|^2 dt$$
$$+ \frac{1}{2} \int_0^T \sum_{j \in \mathcal{J}_{v,c}^M} |s_j^{v,c}(t)|^2 dt$$

s.t.

(y, u, s) satisfies

$$\partial_t y + \partial_x F(y) = G(y),$$

$$R(y(0), y(1), u, s) = 0, \quad y(x, 0) = y_0$$

$$\Xi := \{(y, u, s) : \underline{y}_i \leq y_i \leq \bar{y}_i, \underline{u}_i \leq u_i \leq \bar{u}_i, i \in \mathcal{I}, s_j^{v,c} \in \{0, 1\}\}.$$

Gas networks: A hierarchy of models

$$\begin{aligned}\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho v) &= 0 \\ \frac{\partial}{\partial t}(\rho v) + \frac{\partial}{\partial x}(p + \rho v^2) &= -\frac{\lambda}{2D} \rho v |v| - g \rho h' \\ \frac{\partial}{\partial t} \left(\rho \left(\frac{1}{2} v^2 + e \right) \right) + \frac{\partial}{\partial x} \left(\rho v \left(\frac{1}{2} v^2 + e \right) + p v \right) &= -\frac{k_w}{D} (T - T_w)\end{aligned}$$

- Constitutive law $p = R \rho T z(p, T)$.
- ρ density, v velocity, T its temperature and p the pressure.
- g gravitational constant, $h' = h'(x)$ slope of the pipe, λ friction coefficient of the pipe,
- D diameter, k_w heat coefficient, $T_w = T_w(x)$ temperature of the wall,

Reductions to isothermal eqns.

The isothermal Euler equations

$$\begin{aligned}\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho v) &= 0 \\ \frac{\partial}{\partial t}(\rho v) + \frac{\partial}{\partial x}(p + \rho v^2) &= -\frac{\lambda}{2D}\rho v |v| - g\rho h'\end{aligned}\tag{ISO1}$$

together with $p = R\rho T z(p)$ mit $z(p) = 1 + \alpha p$.

We put $q = \rho v$ and assume for simplicity $c^2 \rho = p$. $z = h'$ is the slope .

Semilinear approximations

For constant $z(p) = z_0$, the speed of sound is $c = \sqrt{\frac{p}{\rho}}$. Hence,

$$p + \rho v^2 = p \left(1 + \frac{v^2}{c^2} \right)$$

For small velocities $|v| \ll c$ we have $\frac{\partial}{\partial x}(\rho v^2)$ small and, hence,

$$\begin{aligned} \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho v) &= 0 \\ \frac{\partial}{\partial t}(\rho v) + \frac{\partial p}{\partial x} &= -\frac{\lambda}{2D} \rho v |v| - g \rho h' \end{aligned} \tag{ISO2}$$

If also $\frac{\partial}{\partial t}(\rho v)$ is small, then

$$\begin{aligned} \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho v) &= 0 \\ \frac{\partial p}{\partial x} &= -\frac{\lambda}{2D} \rho v |v| - g \rho h'. \end{aligned} \tag{ISO3}$$

Further reductions up to algebraic equations

With $h' = 0$ follows even

$$\begin{aligned}\frac{\partial p}{\partial x} &= -\frac{\lambda}{2D}\rho v |v| \\ \frac{\partial p}{\partial t} &= \frac{1}{2}\sqrt{\frac{DRTz_0}{\lambda}} \frac{\frac{\partial^2}{\partial x^2}p^2}{\sqrt{|\frac{\partial}{\partial x}p^2|}}\end{aligned}\tag{ISO3P}$$

For stationary precesses and $z = z_0$ we obtain the algebraic system

$$\begin{aligned}\frac{\partial}{\partial x}(\rho v) &= 0 \\ \frac{\partial p}{\partial x} &= -\frac{\lambda}{2D}\rho v |v|\end{aligned}\tag{ISO4}$$

or

$$p(x) = \sqrt{p_{in}^2 - \frac{\lambda c^2 x}{2D}\rho v |\rho v|}\tag{1}$$

Model adaptivity needed

Given the flow state $y(x, t)$ for some (sampled, measured) (x, t)

- decide which model is to be used on each edge of the graph (slow flow → algebraic, linear or semi-linear model, otherwise the full set of equations by a discrete decision process)
- choose the appropriate coupling conditions
- generate a 'multiscale' model
- obtain a stationary state
- and solve the corresponding forward simulation problem on the entire network
- this is then used as warm-start for the optimal control problems

Network notation

Let $G = (V, E)$ denote the graph of the gas network with vertices (nodes) $V = \{n_1, n_2, \dots, n_{|V|}\}$ and edges $E = \{e_1, e_2, \dots, e_{|E|}\}$. Node indices are denoted $j \in \mathcal{J}$, $|\mathcal{J}| = |V|$, while edges are labelled $i \in \mathcal{I}$, $|\mathcal{I}| = |E|$. For the sake of uniqueness, we associate to each edge a direction. Accordingly, we introduce the edge-node incidence matrix

$$d_{ij} = \begin{cases} -1, & \text{if node } n_j \text{ is the left node of the edge } e_i, \\ +1, & \text{if node } n_j \text{ is the right node of the edge } e_i, \\ 0, & \text{else.} \end{cases}$$

The semi-linear network model

$$\partial_t p_i(x, t) + \frac{c_i^2}{a_i} \partial_x q_i(x, t) = 0$$

$$\partial_t q_i(x, t) + \partial_x p_i(x, t) = -\frac{\lambda c_i^2}{2Da_i^2} \frac{q_i(x, t) \text{abs} q_i(x, t)}{p_i(x, t)},$$

$$g_j(p_i(n_j, t), q_i(n_j, t)) = u_j(t), \quad d_j = 1, \quad i \in \mathcal{I}_j,$$

$$p_i(n_j, t) = p_k(n_j, t), \quad \forall i, k \in \mathcal{I}_j, \quad d_j > 1,$$

$$\sum_{i \in \mathcal{I}_j} d_{ij} q_i(n_j, t) = 0, \quad d_j > 1,$$

$$s_j^v(t) \left[p_i(n_j, t)_{i \in \mathcal{I}_j^-} - p_k(n_j, t)_{k \in \mathcal{I}_j^+} \right] + (1 - s_j^v(t)) q_i(n_j, t)_{i \in \mathcal{I}_j^-} = 0, \quad j \in \mathcal{J}_v \quad (1)$$

$$s_j^c(t) \left[u_j - C \left(\left(\frac{p_k(n_j, t)}{p_i(n_j, t)} \right)^{\text{sign}(q_k(n_j, t))\kappa} - 1 \right) \right]$$

$$+ (1 - s_j^c(t)) \left[p_i(n_j, t)_{i \in \mathcal{I}_j^-} - p_k(n_j, t)_{k \in \mathcal{I}_j^+} \right]$$

$$p_i(x, 0) = p_{i,0}(x), \quad q_i(x, 0) = q_{ij}(x),$$

$$i \in \mathcal{I}, \quad x \in (0, \ell_i), \quad t \in (0, T).$$

The optimal control problem

$$\begin{aligned}
 \min_{(p,q,u,s) \in \Xi} I(p,q,u) &:= \sum_{i \in \mathcal{I}} \int_0^T \int_0^{\ell_i} l_i(p_i, q_i) dx dt + \frac{\nu}{2} \sum_{j \in \mathcal{J}^s \cup \mathcal{J}_c} \int_0^T |u_j(t)|^2 dt \\
 &\quad + \frac{1}{2} \int_0^T \sum_{j \in \mathcal{J}_{v,c}^M} |s_j^{v,c}(t)|^2 dt \\
 &\quad s.t. \\
 &\quad (p,q,u,s) \text{ satisfies (1),}
 \end{aligned}$$

$$\Xi := \{(p,q,u,s) : \underline{p}_i \leq p_i \leq \bar{p}_i, \underline{q}_i \leq q_i \leq \bar{q}_i, \underline{u}_i \leq u_i \leq \bar{u}_i, i \in \mathcal{I}, s_j^{v,c} \in \{0,1\}\}$$

We now consider the time discretization such that $[0, T]$ is decomposed into break points $t_0 = 0 < t_1 < \dots < t_N = T$ with widths $\Delta t_n := t_{n+1} - t_n, n = 0, \dots, N-1$. Accordingly, we denote $p_i(x, t_n) := p_{i,n}(x), q_i(x, t_n) := q_{i,n}(x), n = 0, \dots, N-1$. We consider a semi-implicit Euler scheme which takes p_i in the friction term in an explicit manner.

The time discrete model

$$\begin{aligned}
 \frac{1}{\Delta t} p_{i,n+1}(x) + \frac{c_i^2}{a_i} \partial_x q_{i,n+1}(x) &= \frac{1}{\Delta t} p_{i,n}(x), \quad x \in (0, \ell_i), i \in \mathcal{I} \\
 \frac{1}{\Delta t} q_{i,n+1}(x) + \partial_x p_{i,n+1}(x) &= -\frac{\lambda c_i^2}{2D_i a_i^2} \frac{q_{i,n+1}(x) \text{abs} q_{i,n+1}(x)}{p_{i,n}(x)} \\
 &\quad + \frac{1}{\Delta t} q_{i,n}(x), \quad x \in (0, \ell_i), i \in \mathcal{I} \\
 g_j(p_{i,n+1}(n_j), q_{i,n+1}(n_j)) &= u_{j,n+1}, \quad i \in \mathcal{I}_j, j \in \mathcal{J}^S \\
 p_{i,n+1}(n_j) &= p_{k,n+1}(n_j), \quad \forall i, k \in \mathcal{I}_j, j \in \mathcal{J}^M \\
 \sum_{i \in \mathcal{I}_j} d_{ij} q_{i,n+1}(n_j) &= 0, \quad j \in \mathcal{J}^M, \\
 s_{j,n+1}^v \left[p_{i,n+1}(n_j)_{i \in \mathcal{I}_j^-} - p_{k,n+1}(n_j)_{k \in \mathcal{I}_j^+} \right] &+ (1 - s_{j,n+1}^v) q_{i,n+1}(n_j)_{i \in \mathcal{I}_j^-} = 0, j \in \mathcal{J}^I \\
 s_{j,n+1}^c \left[p_{i,n+1}(n_j)_{i \in \mathcal{I}_j^-} u_j - p_{k,n+1}(n_j)_{k \in \mathcal{I}_j^+} \right] &+ (1 - s_{j,n+1}^c) \left[p_{i,n+1}(n_j)_{i \in \mathcal{I}_j^-} - p_{k,n+1}(n_j)_{k \in \mathcal{I}_j^+} \right] = 0, j \in \mathcal{J}^C \\
 p_{i,0}(x) &= p_{i0}(x), \quad q_{i,0}(x) = q_{i0}(x), \quad x \in (0, \ell_i), i \in \mathcal{I}.
 \end{aligned} \tag{2}$$

Time-discrete optimal control problem

We then obtain the optimal control problem on the time-discrete level:

$$\min_{(p,q,u,s) \in \Xi} l(p, q, u, s) := \sum_{i \in \mathcal{I}} \sum_{n=1}^N \int_0^{\ell_i} l_i(p_{i,n}, q_{i,n}) dx + \frac{\nu}{2} \sum_{j \in \mathcal{J}^S \cup \mathcal{J}_c} \sum_{n=1}^N |u_j(n)|^2 \\ + \frac{1}{2} \sum_{n=1}^N \sum_{j \in \mathcal{J}_{v,c}^M} |s_{j,n}^{v,c}|^2$$

s.t.

(p, q, u, s) satisfies (2).

$$l_i((p_{i,n}, q_{i,n}))(x) := \frac{1}{2} |p_{i,n}(x) - p_{i,n}^d(x)|^2 + |q_{i,n}(x) - q_{i,n}^d(x)|^2, x \in (0, \ell_i), i \in \mathcal{I}.$$

Instantaneous control

$$\min_{(p,q,u,s) \in \Xi} I(p, q, u) := \sum_{i \in \mathcal{I}} \int_0^{\ell_i} l_i(p_i, q_i) dx + \frac{\nu}{2} \sum_{j \in \mathcal{J}^S \cup \mathcal{J}_c} |u_j|^2 + \frac{1}{2} \sum_{j \in \mathcal{J}_{v,c}^M} |s_{j,n}^{v,c}|^2$$

s.t.

$$\beta_i p_i(x) + \partial_x q_i(x) = f_i^1, \quad x \in (0, \ell_i), \quad i \in \mathcal{I}$$

$$\alpha_i q_i(x) + \partial_x p_i(x) + g_i(x; q_i(x)) = f_i^2, \quad x \in (0, \ell_i), \quad i \in \mathcal{I}$$

$$g_j(p_i(n_j), q_i(n_j)) = u_j, \quad i \in \mathcal{I}_j, \quad j \in \mathcal{J}^S$$

$$p_i(n_j) = p_k(n_j), \quad \forall i, k \in \mathcal{I}_j, \quad j \in \mathcal{J}^M$$

$$\sum_{i \in \mathcal{I}_j} d_{ij} q_i(n_j) = 0, \quad j \in \mathcal{J}^M$$

$$s_j^v \left[p_i(n_j)_{i \in \mathcal{I}_j^-} - p_k(n_j)_{k \in \mathcal{I}_j^+} \right] + (1 - s_j^v) q_i(n_j)_{i \in \mathcal{I}_j^-} = 0, \quad j \in \mathcal{J}_v$$

$$s_j^c \left[p_i(n_j)_{i \in \mathcal{I}_j^-} u_j - p_k(n_j)_{k \in \mathcal{I}_j^+} \right] + (1 - s_j^c) \left[p_i(n_j)_{i \in \mathcal{I}_j^-} - p_k(n_j)_{k \in \mathcal{I}_j^+} \right] = 0, \quad j \in \mathcal{J}_c$$

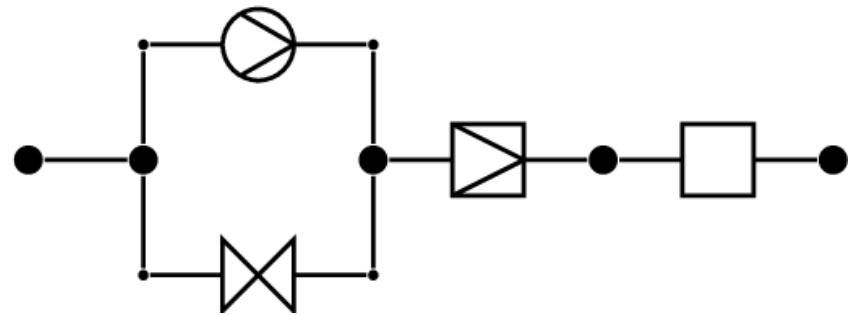
Master-slave decomposition

Given the flow state $y(x, t)$ for some (sampled, measured) (x, t) and given an appropriate multi-scale model simulation

- solve the discrete optimal control problem and obtain a switching structure s (master)
- with this s , solve the continuous optimal control problem (slave) (using e.g. domain decomposition)
- check feasibility of the solutions (need measure for mismatch)
- convey the result to the master
- prove convergence

Consortium in Germany

<http://trr154.fau.de/index.php/de/>



There are currently 75 articles on the server



Mathematical Modelling,
Simulation and Optimization Using
the Example of Gas Networks